

Towards Wireless Control in Industrial Process Automation

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Wireless sensors and networks are today only occasionally used in control loops in the
2 process industry. With the current rapid developments in embedded and high-performance com-
puting, wireless communication, and cloud technology, drastic changes in the architecture and
4 operation of industrial automation systems seem more likely to happen than ever before. These
changes are driven by ever growing demands on production quality and flexibility. However,
6 there are several research obstacles to overcome: The radio communication environment in
the process industry is often troublesome as the environment is frequently cluttered with large
8 metal objects, moving machines and vehicles, and processes emitting radio disturbances [1],
[2]. Successful deployment of a wireless control system in such an environment requires careful
10 design of communication links and network protocols, as well as robust and re-configurable
control algorithms.

12 Based on some examples from the Iggesund paper mill in Sweden, with a long history,
see “Iggesund Mill History”, we will in this paper discuss some recent developments towards
14 wireless control in industrial process automation. Despite major scientific progress over the last
couple of decades in wireless networked control [3] with, for instance, important results on
16 how plants can be stabilized and optimized over packet-switched networks [4] surprisingly little
impact has been reported on commercial implementations in the process industry. We argue
18 here that a more integrated approach to the design of these systems is needed, exploring trade-
offs between the communication and control systems in a systematic way. Existing standardized
20 industrial communication protocols, such as ISA-100 and WirelessHART, provide a large degree
of freedom for the users including many tuning parameters, but developing co-design methods
22 utilizing this freedom is still needed [5]. A brief survey of recent advances on wireless control
is summarized in “Advances in Wireless Control”.

The outline of this paper is as follows. First we describe a possible future control architecture and detail some key challenges in next generation process automation. The Iggesund paper mill is then introduced as a case study. It is used throughout the paper to illustrate the considered communication and control problems. Results are presented on modelling of radio channels in an industrial environment. The joint behaviour of multiple wireless sensor–sensor and sensor–gateway channels is discussed and models useful for routing data packets are proposed. Energy harvesting in wireless sensor networks is then demonstrated on the industrial process. Event-based control for wireless systems is investigated for both feedback and feedforward control, followed by a proof-of-concept implementation of wireless control at Iggesund. Finally, in the last section, conclusions are drawn.

Challenges in next generation process control

With the recent developments towards Internet-of-Things (IoT), we can expect that future devices and systems can much more seamlessly communicate. The most immediate effects are seen in data analytics, where new devices can collect data online and feed it into the cloud without going through a control system. Once in the cloud almost “unlimited” computing power can be applied for processing the data for various purposes such as, for instance, predictive or prescriptive maintenance. It is, however, clear that this will have an effect not only on analytics but also on process control and other process operations.

Inspired by the development in mobile platforms such as iPhone and Android it is reasonable to assume that most functions that are not time- or safety critical could become available as “apps” in an automation platform. Today we often have large monolithic software systems for each layer of the classical automation pyramid, such as for process control, manufacturing execution system (MES), and enterprise resource planning (ERP). Instead, these functions may be broken down into smaller components that seamlessly communicate within one “app” platform. This would also make it easier for smaller players who only provide a limited or smaller scope of functionality to participate in the market.

ExxonMobil, as one of the world’s largest process companies, in 2016 clearly communicated its vision towards a future control architecture through a set of presentations [6]. Their vision states concretely that a future control system should be built on distributed control nodes (DCN) that are dedicated single-channel I/O modules with control capability connected to a real-time data service bus. Furthermore, the operations platform should be open and use open-source software. This would enable a much easier revamping of current distributed control system (DCS) architecture philosophy, which in their view is both complex and expensive. By adopting this vision, together with the above idea of one common “app” platform, the traditional automation

pyramid, which structurally separates process control, scheduling and planning to their own hierarchical levels, may be replaced by a more flexible paradigm. A somewhat simplified version of the ExxonMobil vision is depicted in Figure 1.

At the lowest level of a control system, there are measurement devices, for instance, sensors and analyzers, as well as actuating devices such as valves and pumps. At this device level the connection to the common real-time bus could be realized through a standardized DCN as suggested by ExxonMobil. More futuristic, however, is to assume that all devices have enough intelligence to handle the connectivity and low level control computations themselves, see, for example [7]. As indicated already above, one interesting question is then where a particular computation should take place. Clearly there will always be a need to carry out some computations with a minimum of latency. Hence we have a trade-off between moving current DCS functionality to the Operations Platform or the DCN/device, as indicated by the arrows in Figure 1.

In this whole discussion a central question to this paper is what role wireless communications will play in this future automation architecture. In Figure 1, the possibility of a wireless gateway is indicated. However, we will in this paper argue that a standard choice for the DCN and other intelligent devices would be to use wireless communications, even for situations requiring fast communications. As has been pointed out by many before us [2], [8], [9], there are multiple potential advantages with wireless instead of wired communications such as cost savings in cables and installation as well as more flexible operation. The rest of this paper will be devoted to investigating the feasibility and reliability of the use of wireless communications in process applications with a particular focus on the pulp and paper industry.

From a system perspective there are also several challenges in order to maintain high availability and safe control functions. From an engineering perspective the control applications have to support online changes and the system architecture needs to deal with seamless reconfiguration, to distribute new applications while ensuring system integrity to name a few. Furthermore, on the real-time bus, new challenges arise in order to deal with different real-time traffic classes, video streams, as well as best-effort traffic in a system architecture such as the one in Figure 1. In addition to this, redundancy is required in order to meet the industry demand on the availability of the control system, and to take the processes into safe states in case of errors that cannot be automatically recovered, without creating isolated network functions that are executing (partly) blindly.

Iggesund paperboard machine case study

2 The Iggesund Mill is a fully integrated pulp and paperboard mill with a long history, see
“Iggesund Mill History”. The pulp mill is the area where the large chimneys are located, in the
4 upper center of Figure 2. The paperboard mill and the coating kitchen is the building complex in
the middle of Figure 2. There are two paperboard machines, see Figure 3, and the products that
6 are manufactured are primarily for packaging and graphic purposes, which require high quality.
In order to obtain a paperboard of the quality produced at the Iggesund Mill, there is also a
8 coating kitchen that delivers coatings which are used to coat the paperboard to make it smooth
and even, and hence a good surface for printing.

10 Throughout a recent three year long project period, several real live tests have been
conducted to evaluate wireless control in the industrial environment of the factory. These tests
12 were carried out mainly at the coating kitchen, where there are two starch cookers. The starch
production is one important ingredient when mixing and preparing the coating of the paperboard.
14 The starch is providing the finish and color of the paperboard which is used for exclusive
packaging of, for example, whiskey, perfumes, and chocolate. This process is delivering coating
16 to both paper machines and the final quality of the paperboard is depending on a constant supply
of high quality coating. The cookers are used to boil the starch, which is subsequently used in the
18 manufacturing of the different coatings. During the experiments, only one cooker was used. The
main reason for using only one of the boilers as a test bed in the wireless control experiments was
20 that we could implement the wireless outbreak on one cooker while in the meantime continue
with normal production on the other, and thus the experiments did not disturb the production
22 at the paperboard machines. The process in the cookers works so that silo H1 is a buffer for
the starch powder. A picture of the silo H1 is shown in the upper left part of Figure 4. From
24 there, the powder is transported to a storage hopper with a level regulator to ensure the same
degree of filling in the dosing screws. It is in the mixing tank the dry powder mixes with water.
26 The picture at the bottom left part of Figure 4 shows this process, which is controlled via a
concentration regulator. The mixture is then pumped into the steam ejector where steam is added
28 to boil the starch. The starch boiling process is controlled by a temperature regulator. After that,
water is added again to get the correct dry content on the final product. A picture of the process
30 where the starch is boiled is shown in the upper right corner of Figure 4. The starch cooking
is a batch process which is started and stopped automatically by the level in the storage tanks.
32 The picture at the bottom right of Figure 4 shows these storage tanks.

A wireless control architecture for the starch cooker

2 Figure 5 shows a proposed wireless control architecture for the starch cooker process of the
Iggesund pulp and paperboard mill. The architecture consists of multiple wireless feedback
4 loops involving sensors (S_j) and actuators (A_j). From left to right in Figure 5 the cooker works
as follows: Water from the mix water tank, the level of which is controlled by (S_1, A_1), is mixed
6 with starch powder distributed through the mix funnel. The properties of the so obtained starch-
water mixture is governed by the concentration control loop (S_2, A_2) and the coarse flow control
8 loop (S_3, A_3). The mixture is cooked using a steam injector, which is temperature controlled
by (S_4, A_4). The concentration of the starch solution is further diluted by the fine flow control
10 loop (S_5, A_5) after which a mixing and pressure control loop, governed by (S_6, A_6), is making
the final touch before the starch solution is sent to the storage tank. In our wireless setup, all
12 control actions are calculated at the actuators in a distributed fashion and the sensor- and actuator
information is sent to the gateways (GW) for further distribution to the operators.

14 Modeling of radio channels in industrial environment

When a wireless environment is static, the wireless link design is fairly straightforward,
16 even if Line-of-Sight between the transmitting node and the receiving node cannot be obtained.
It is then just a matter of selecting the appropriate number of sensor nodes, good locations and/or
18 adjusting the transmit power. However, even if an industrial environment at a first glance looks
static, it is very seldom so over a longer time horizon (several minutes and hours).

20 In the literature, typical indoor channels are found to be well described by either log-
normal (LN), Rayleigh, Rice, Nakagami- m , (Gamma (G) in the power domain), or, sometimes,
22 even Weibull distributions [1], [10]–[12]. The distribution that fits the received data best depends
on the environment and the degree of motion around the communicating sensor nodes and the
24 observation interval. For a comprehensive overview of radio channel characteristics in indoor
and industrial environments, see, for example., [11]–[13] and the references therein. Furthermore,
26 previous studies have observed that temporal channel variations in WSNs with stationary nodes,
that is, both the transmitting and receiving antennas are stationary, typically follow a Rician or
28 Nakagami- m distribution [1], [11], [14].

Characterizing channel gain variability

30 To obtain an accurate representation of the radio environment at the paper mill in Iggesund,
numerous point-to-point measurements were performed at different positions along the paper
32 mill production line as well as in the starch cooker environment. In addition to these point-to-

point measurements, numerous rig measurements were conducted. (For the rig measurements the location of the transmitter was fixed whereas the receiver was moved in a controlled direction in space.) The very common assumption used in cellular communications where radio links are subject to Rayleigh fading, which typically arises when a receiver is moving through a standing wave pattern with multiple scatterers in the vicinity, was confirmed by our numerous measurements from static environments in Iggesund [15]. However, our extensive sensor node-to-sensor node measurement campaigns, conducted at Iggesund and at two other process industries, confirm that static channels are rare, particularly when observing the radio environment over several minutes and hours, see [15], [16].

The typical situation in industrial environments, like the one in Iggesund, is that wireless channel variability in node-to-node links is caused by objects moving in the vicinity of, or in between, the sensor nodes. Examples of such a channel gain variability at the finish line of the paper mill and at the cooker environment are illustrated in Figure 6a and Figure 6b, respectively.

A closer look at Figure 6a reveals that the channel gain can vary with some 20-30 dBm and stay in a higher or lower dB region for several minutes and even hours. In Figure 6a the link variability is caused by a crane, located in the ceiling of the building, moving finished high quality paper from the roll up section to the floor and from one location on the floor to another where they are temporarily stored for later cutting and long term storage. In this case the intermediate storage of the paper rolls shadowed the radio link between the two nodes causing a significant change in the channel gain, see Figure 7a. In the time interval [4.5 – 8.5] hours in Figure 6a the intermediate storage on the floor next to the roll up section was cleared and the channel gain increased for a period of several hours. A similar channel gain variability was observed at several other locations at the paper mill. However, at the starch cooker location, see Figure 7b, the channel gain variability was primarily caused by people moving in the narrow aisle close to the sensor node locations, see Figure 6b. Here the variability was in the range of 10-20 dBm. This indicates that a careful channel modelling is required, should energy efficient and low latency communications be attained, which constitute a prerequisite for low latency controller design.

Parameter estimation

When taking the variability of several links into account, Maximum Likelihood estimation of the model parameters reveals that neither Rayleigh or Rice, nor log-Normal distributions are solely adequate for describing the fading characteristics in a typical paper mill environment, see Figure 8. It is clear that the Nakagami-lognormal (Gamma-lognormal (GLN) in the power domain) compound distribution gives the best fit to the link measurement data acquired from the extensive measurement campaign conducted at the paper mill. Figure 8a depicts the estimated and

empirical cumulative power level distribution in dB whereas Figure 8b illustrates the theoretical and empirical average bit error rates (BER) for different distributions. Evidently, selecting the wrong fading distribution will have a detrimental effect on both energy expenditure and BER. In Figure 8, a one component compound distribution was considered. However, when performing a more in-depth identification based on the Iggesund measurement data over different time horizons, two fading components, (see “Radio Model Selection”) are frequently required as is illustrated in Table 1. Measurement campaigns conducted at other industrial sites show that even three components might be required in some cases. From Table 1 we observe that for one hour segments one component suffices in 59% of the cases. In those one component cases, a GLN channel model fits the data best in 39% of the cases, whereas in 20% of the cases a G channel model is sufficient. In 34% of the total cases a two component compound model consisting of either G or GLN combinations turns out to be the best choice.

The situation is similar for four hour segments, but in this case a two component compound model is somewhat less frequent. For the sixteen hour segments, only in 15% of the cases a two component compound model was appropriate. We can thus conclude that in most cases a one component GLN model is a good description of the link variability at the Iggesund site. In other cases, such as for the Sandviken rolling mill measurement campaign, a two component model was the most appropriate choice for the 16 hour segments. These findings suggest that before a wireless control network is to be deployed at a new industrial site, a measurement campaign should be conducted to determine the required complexity of the fading distributions. Then both better BER and energy expenditure figures can be obtained.

Modeling joint behavior of radio channels in industrial environments

In this section, we extend the analysis of the radio channel measurements from the previous section and study the joint behavior of radio links. Specifically, by partitioning the link measurements into volatile and quiescent periods using hidden Markov models (HMM), we identify which links that are likely to experience severe fading simultaneously. The study is motivated by emerging routing protocols for wireless sensor networks (WSNs) where multipath diversity has been considered a key for achieving a timely data transfer [17].

These protocols transmit multiple copies of each data packet over parallel paths and this technique is most effective if transmission failures over the paths are uncorrelated. For instance, if a single event affects the quality of several paths, then there is little gain from the multipath diversity. In a scenario where a sensor node has multiple neighbors, from which a subset is to be selected as relaying nodes, the gain from the multipath diversity is increased if the selection process uses information on correlations in link quality among its neighbors. In this section we

outline an algorithm for detecting such correlations. We also demonstrate the performance of the algorithm on measurements of channel gains obtained from a network of nodes deployed in the vicinity of the previously mentioned starch cooker. The results show that it is common that some links undergo joint changes in link quality and we describe how this information could be incorporated into the design of multipath routing protocols.

Measurements

For the purpose of the analysis in this section, we focus on measurements obtained from seven wireless sensor nodes. These were deployed in the vicinity of the starch cooker and Figure 9 illustrates a map of the deployment area which included heavy machines and a large amount of metal objects.

In Figure 9, we picture a scenario where the node marked RX is a sensor node that is listening to transmissions from six of its neighbours that are all closer to the intended gateway, which is not depicted in the figure. The objective of the RX node is to select a subset of these neighbours as relaying nodes and, as will be described in more detail below, the subset should be selected so that the gain from the multipath diversity is increased.

The transmissions were performed in a round-robin fashion where each of the nodes with label 1-6 sent a packet to the RX node which recorded the received signal strength (RSS) of the incoming transmissions. Each node sent a packet every 0.125 seconds and measurements were conducted for three hours. A short segment of the resulting time series is illustrated in Figure 10.

As described in the previous section, the fading distribution of each link switched abruptly between volatile periods and more quiescent periods, where the channel gain could vary on the order of 20 dB in the former case. Moreover, initial studies of the measurements showed that, for each link, the volatile periods had a roughly similar spectrum. Hence, to detect changes in volatility of the monitored links, we propose a two state HMM where each state generates observations from an autoregressive (AR) process. For future reference, we let $\hat{z}_{l,t}$ denote the state of link l at time t , where $\hat{z}_{l,t} = 1$ indicates the volatile fading state and $\hat{z}_{l,t} = 0$ the quiescent fading state. In [18], Rabiner outlined an algorithm for inference of such models and we summarize the most important steps in “Data Generation Model”. Finally, the inferred state sequence, which partitions each link into periods of volatile and quiescent behavior, will be used to identify links that are likely to experience severe fading simultaneously.

Results

Movement in the vicinity of the nodes mostly consisted of personnel that were walking along the paths that are marked by double dashed lines in Figure 9. Since the nodes were positioned in two clusters, where we for future reference let cluster 1 denote nodes 1-4 and cluster 2 denote nodes 5-6, passing personnel induced time varying shadow fading that often affected all the links in a cluster. However, due to the spatial separation between the clusters, it was unlikely that both of them were shadowed simultaneously.

In Figure 10, the background color indicates the estimated state sequence, \hat{z}_l , from the HMMs. As expected, there is a tendency for the nodes in cluster 1 to have overlapping volatile regions. The same tendency can be observed for cluster 2. However, the volatile regions between nodes from different clusters show more sporadic overlap.

Table 2 lists the empirical probabilities, $o_{i,j}$, that \mathbf{x}_j is in the volatile state given that \mathbf{x}_i is in the volatile state, which can be computed as,

$$o_{i,j} = \frac{\sum_{t=1}^T \hat{z}_{i,t} \hat{z}_{j,t}}{\sum_{t=1}^T \hat{z}_{i,t}}. \quad (1)$$

The blue and red fields highlight the sparsity of the table which indicates that, for instance, if \mathbf{x}_1 is in the volatile state, then it is likely that \mathbf{x}_2 , \mathbf{x}_3 and \mathbf{x}_4 are also in the volatile state. However, it is less likely that \mathbf{x}_5 or \mathbf{x}_6 is in the volatile state.

In summary, by using HMMs, a sensor node can identify correlations in link quality among its neighbours. This information can potentially be useful in a scenario where the node wants to transmit data to a sink node using a subset of these neighbours as relaying nodes. In this case the robust choice, in the sense that the selected paths drop packets independently, is to send the packet to the neighbors which exhibit no or weak correlation in link quality.

Energy harvesting in wireless networks

Employing many additional sensors to a large plant can have several significant advantages such as enabling more complex signal processing and control algorithms due to more information being available. Using wireless sensors and appropriate routing protocols as described above already simplifies this process by avoiding wires for information flow. Flexibility when adding wireless sensors to the plant can further be enhanced if the sensors do not have to be connected to the electricity grid but instead are powered using energy harvesting. For instance, at the starch cooker at Iggesund paper mill, several energy sources such as hot pipes or tanks, rotating or vibrating parts or the lighting can be used to extract energy to power wireless sensors.

In order to study the energy harvesting capabilities at Iggesund paper mill, several wireless energy harvesting sensors were employed. Some sensors, such as the one shown in Figure 11a were equipped with small solar cells to harvest energy from the lighting. Since some mixing tanks and pipes get very hot, the resulting large temperature gradients can be used to harvest energies using Peltier elements such as shown in Figure 11b. The harvested energy was stored in a local rechargeable battery to be used for data transmission immediately or at a later stage.

Then, a simple algorithm was used to control the sensors: measurements should be submitted every 1 to 3 seconds if sufficient energy is available in the sensor's battery or, otherwise, as soon as enough energy is available again. Figure 12 shows the time between consecutive packets received from a wireless sensor located close to node 4 in Figure 9 for a measurement campaign over several hours. Here, the harvested energy apparently varies periodically since the pipe delivers a product of a reoccurring batch process, of slightly more than one hour length. Since the energy is harvested from a hot pipe, the amount of harvested energy significantly depends on the temperature of the pipe, which varies periodically due to the batch process. Thus, when the pipe cools down after the necessary amount of hot liquid has been delivered for the current batch, less energy can be harvested and the time between sent packets increases as observed in Figure 12. Large time gaps between consecutive packets, and long periods of time where no packets can be sent due to a lack of harvested energy, are highly undesirable in practical settings. One method to improve this situation is to derive better algorithms to allocate the available harvested energy. As for the energy harvesting scenario illustrated in Figure 12, information or a model of the underlying batch process should be used to predict and plan for the available harvested energy over time so that, for instance, the maximal time between consecutive packets is minimized.

To model the available energy over time, first denote the harvested energy at sensor m and time slot k by $H_m(k)$. Several methods exist to model the harvested energy such as Markov chains, motivated by empirical measurements reported in [19]. For instance, for the harvesting process underlying in Figure 12, additional information such as the temperature of the liquid in the pipe can be used to derive more accurate models. The energy harvested at time slot k is stored in the battery, and can be used for different tasks such as data transmission in the $k + 1$ -th time slot. Hence, the dynamics of the battery level of sensor m at time $k + 1$ can be described by $B_m(k)$, evolving according to

$$B_m(k + 1) = \min \left\{ B_m(k) + H_m(k) - E_m(k); \hat{B}_m \right\}, \quad (2)$$

where $E_m(k)$ denotes the energy used by sensor m at time k and \hat{B}_m denotes the battery capacity.

This battery model, together with a model for the harvesting process, can then be used to

derive suitable energy allocation policies. For instance, if the harvesting sensor should transmit
 2 data over a fading channel, an optimal energy allocation policy could be derived, that chooses
 suitable transmission energies depending on the battery level and the channel gain in order to
 4 maximize a desired quantity of interest.

Event-based control

In event-based networked control systems sensors transmit only when certain conditions are satisfied. Such systems have been quite widely studied over the last couple of decades, mainly motivated by their lower requirements on communication compared to conventional periodic control, see “Advances in Event-based Control”. In this section, we discuss the event-based control of the starch cooker process with wireless sensors, as illustrated in Figure 5. Especially, we describe how event-based feedback and feedforward control could be implemented for that process.

Let us focus on one specific control loop of the starch cooker, namely, the fine water flow control. The fine water flow is controlled by using sensor S_5 and actuator A_5 in Figure 5 to obtain the desired final starch paste solution. The concentration is possibly disturbed by the change of the steam flow into the steam ejector, or the change of the starch concentration after the screen. Since such a disturbance only slowly affects the final product, it is difficult to mitigate the influence effectively by feedback control. Feedforward compensation is able to adjust the fine water flow rate as soon as the disturbance is detected. To do this, the steam flow and the opening of the steam valve are monitored by the sensor S_4 and the actuator signal A_4 , respectively. Since disturbances act only now and then, it is reasonable to use event-based compensation, that is, to let S_4 and A_4 transmit their sensor and actuator values only when each value changes more than a certain threshold. We illustrate the merit of such an event-based feedforward compensation scheme in this section as well as the event-based feedback control. To mimic a control loop in the starch cooker, let us introduce a continuous-time linear system given by

$$\dot{x}_p(t) = Ax_p(t) + Bu(t) + \tilde{B}w(t) \tag{3}$$

$$y(t) = Cx_p(t) \tag{4}$$

where x_p is the plant state, y the plant sensor output, w the disturbance, and u the control input to the plant. The disturbance w affects the plant through the disturbance dynamics

$$\dot{w}(t) = A_d w(t) + B_d d(t) \tag{5}$$

where d is the external disturbance which can be measured by the disturbance sensor $y_d(t) = C_d d(t)$. For this system, a PI control with discrete sampling is implemented as

$$\begin{aligned}\dot{x}_c(t) &= y(t_k) - r(t) \\ u(t) &= K_p(y(t_k) - r(t)) + K_i x_c(t) + K_f y_d(t_\ell)\end{aligned}$$

where x_c is the integrator state, r the reference (setpoint) signal, and t_k the time of sample k of the event generator of the plant sensor, t_ℓ the time of sample ℓ of the disturbance sensor. Furthermore, K_p and K_i are appropriately tuned proportional and integral gains, respectively. The feedforward gain is denoted K_f . The block diagram of the event-based control system is depicted in Figure 13.

Let us first consider the event-based feedforward control, corresponding to that the event generator in the feedback loop of Figure 13 is periodic. A disturbance event is generated at the sensor when the condition $|y_d(t) - y_d(t_\ell)| \geq \bar{e}_d$ is satisfied, where t_ℓ is the last measurement instance and \bar{e}_d some prespecified event threshold.

Figure 14 shows three simulations of disturbance responses for a first-order system with and without feedforward control, and with PI feedback control in all three cases. Note that we consider periodic samplings of the feedback control loop in all cases. The upper plot shows the disturbance, the middle plot the plant state, and the lower plot the PI control signal. We note that even if the feedforward event generator only transmits nine measurements of the disturbance (red circles in the upper plot), it performs equally well to the continuous-time feedforward control (green). Further discussion on the design of feedforward event-based control is given in [20].

Now instead consider the case when there are no disturbance: $d(t) \equiv 0$ for all $t \geq 0$. Then the system in Figure 13 is a conventional event-based PI control system studied by many authors in the literature [21]–[27]. Some of these works [23], [24], [26] investigate event-based PI control with events generated when the measurement error reaches above a threshold \bar{e} :

$$|y(t) - y(t_k)| \geq \bar{e}.$$

In the thesis [23] and the subsequent paper [24], the performance of PI control with this sampling scheme was evaluated in some industrial control loops at the Iggesund Paperboard. It was demonstrated that with a careful selection of the threshold the sampling may be reduced as much as 90% or more with only a marginal loss of control performance. Figure 15 (which is re-drawn from Figure 3 in [24]) shows step responses for a reject tank.

In Table 3, the results are summarized for three performance measures: integrated absolute control error IAE , integrated squared control error ISE and average overshoot for the negative

and positive steps. The table also gives the communication reduction in percent relative to fast
2 periodic control. More advanced set-point tracking for event-based PI control were developed
in [27] modifying the event-based PIDPLUS [28].

4 An interesting topic for further study is the combination of event-based sampling for the
various sensors in other control architectures, not only feedback and feedforward configurations.

6 **Proof-of-concept implementation at Iggesund Paperboard**

In this section we will present a proof-of-concept implementation at Iggesund Paperboard
8 in the process section introduced in Section IV. The part of the starch cooking section that was
used for the field-trials, is illustrated in Figure 16. The starch is produced in batches. A batch is
10 started when the level of the storage tank reaches a predefined low threshold value and stopped
when the level of the storage tank reaches the high threshold value. During the week when we
12 controlled the starch cooking process, the production rate was set to 1500 kg/h. A typical batch
was running for approximately one hour and then it was stopped for 2-3 hours depending on
14 the quality of the paperboard produced.

A separate process controller was installed in parallel with the existing control system to
16 have a fall back solution, should any failures during the experiments arise. The control loops
were closed using both wireless sensors (S_4 , S_5 , S_6) and wireless actuators (A_4 , A_5 , A_6), see
18 Figure 16. The control loops were implemented in the ABB AC800M controller using standard
PID controllers with the same control parameters as in the existing control system.

20 Furthermore, the wireless system was equipped with a deterministic failure detection
feature, and therefore, the additional process controller would be able to signal to the normal
22 control system to take over in case of a detected error. The wireless actuators would also detect
such an error at the same time as any of the other communication peers in the system, thus being
24 able to electrically switch back the control of the valves to the normal control system. It might
seem to be ambitious to implement such functionality to conduct experiments for research, but
26 it was required for us to conduct measurements and control 24 hours a day for five calendar
days without having researchers stand-by all the time to manually restore production in case of
28 a failure.

The additional process controller, AC800M from ABB, was connected to a gateway in the
30 process via Profinet IO, utilizing an existing fiber between the process and the marshalling room
where the control equipment was installed. In the process, we installed the wireless instruments
32 and the wireless actuators and connected them to the existing valves and instrumentation using
4-20mA interfaces. The gateway and the field devices were realized by assembling two off-the-

shelf evaluation boards in an IP67 enclosure as shown in Figure 17.

2 Challenges with existing industrial wireless sensor network standards such as Wire-
lessHART or ISA100 for wireless control has previously been identified [29]. Therefore solutions
4 to overcome limitations such as, for example, real-time up-links, seamless recovery in case of
link failures, as well as diagnostics to take the end-nodes into a safe state in a timely manner
6 in case of communication errors, has been proposed and implemented. One such solution is
Realflow [30] that has been used in this proof-of-concept implementation, as well as a new time
8 synchronization protocol [31] to have more precise Time Division Media Access. In addition,
solutions to enable several concurrent data flows with different priorities have been implemented
10 to have a deterministic communication network supporting on-line changes and topology changes
without any deadline misses in the real-time communication paths, which is required for control
12 applications.

Consider the flow control depicted in Figure 18. In the beginning of the batch sequence,
14 just before 21:00, the flow controller is enabled to keep a water flow of 41 liters/minute. At this
moment the control valve of the pressure controller is opened to 50% to flush out remainders of
16 starch from the previous batch as can be seen in Figure 19. In parallel with starting the heating
of the boiler the pressure controller is enabled to maintain a pressure of 3.3 Bar in the boiler.
18 After that the batch sequence enables a ramp in the output of the control valve to heat the boiler
with steam. When the temperature of the boiler is close to its set-point of 138 degrees Celsius
20 the temperature controller is enabled to maintain the temperature. This can be seen in Figure 20,
the knee on the yellow line some minutes after 21:00.

22 Just before 22:10 the level of the storage tank have reached the upper threshold and the
control valves to the storage tanks are closed and a cleaning process starts. In Figure 18, a
24 flow disturbance is noticed when the pressure valve is opened for cleaning (see Figure 19). The
cleaning process finished at 22:15 and the starch cooking system is ready for another batch when
26 the storage tank level is reaching its lower threshold.

The batch sequence was started approximately every third hour during the five day
28 experiment period. During this period the plant operators could neither identify any significant
differences between the wireless- and Profibus controlled process, nor did the production system
30 detect any deviations with respect to the control limits installed to provide early warning that
the process section would be in need of maintenance. In addition, the safety functionality that
32 would restore operation to the normal production system was never invoked, since there were no
three consecutive communication errors during five day period. Even when comparing production
34 data between the wireless- and normally controlled process, no differences could be discerned.

However, one could observe slightly different variations in the final concentration of the starch.
2 We were told by the operators that they could see such variations every now and then in the
normal production system, and the variations were explained by variations in the density of the
4 ingredients in the storage tank before mixing. This implies that the feeders' duty cycle will feed
a small variation in volume of the ingredients, which varies over time depending on how full
6 the tank is.

All in all, the general conclusion by the operators and the automation engineers was
8 that they could not tell if the process was controlled with a wireless- or wired technology.
Due to the inherent variations in the quality of the process ingredients we cannot quantify the
10 difference in control performance between the wireless and Profibus controlled process. However,
our experiments indicate that it is indeed feasible to design and implement wireless systems for
12 process control and there is no need to treat them differently than the wired control counterparts,
neither from a quality, nor from a control performance perspective. Furthermore, our wireless
14 control experiment indicates that it is indeed feasible to use wireless control for continuous
operation and production. From an availability perspective this is however a too short a time
16 to draw any general conclusions, but comparing the performance indicators from the wireless
installation with the same performance indicators using the Profibus network suggests that it
18 would be possible to reach the desired availability with a wireless installation.

Conclusions

20 In this paper we have addressed important research problems that are critical to solve before
deploying wireless control systems in the process industry. In large industrial plants such as, for
22 example, a paper mill, information from thousands of sensors would then have to be handled
swiftly over wireless links. We have addressed the importance of having a correct characterization
24 of the radio environment, the use of suitable network protocols for routing sensor information to
the gateways, efficient use of harvested energy from the environment, as well as the use of robust,
26 possibly event based, and reconfigurable control algorithms. Furthermore, we have deployed a
wireless networked control system addressing these aspects at the Iggesund Paperboard papermill.
28 Long term tests were conducted on one of the mill's starch cookers during normal production
over five consecutive days. The tests were very successful and the operators could not distinguish
30 the wireless control system from the wired, which suggests that it is indeed possible to replace
wired control systems with wireless, even in a complex industrial environment.

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Neander, Tommy Norgren, Tomas Olofsson, Jonathan Styrud and Junfeng Wu.

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measurements and wireless control tests on the paper mill's starch cooker during normal
8 production.

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TABLE 1. Obtained number of mixture components (Comp) in % after ML-optimization over one hour (1H), four hour (4H), and sixteen hour (16H) time segments acquired at Iggesund Paperboard in Sweden. Models identified and validated based on received signal strength (RSS) power measurements were, (see, “Radio Model Selection”): Gamma (G) and/or gamma – lognormal (GLN) compound models. (L) is lost packets, that is, packets where received signal strength (RSS) data could not be retrieved. Total number of time segments: 92 (46) for 1H and 4H (16H).

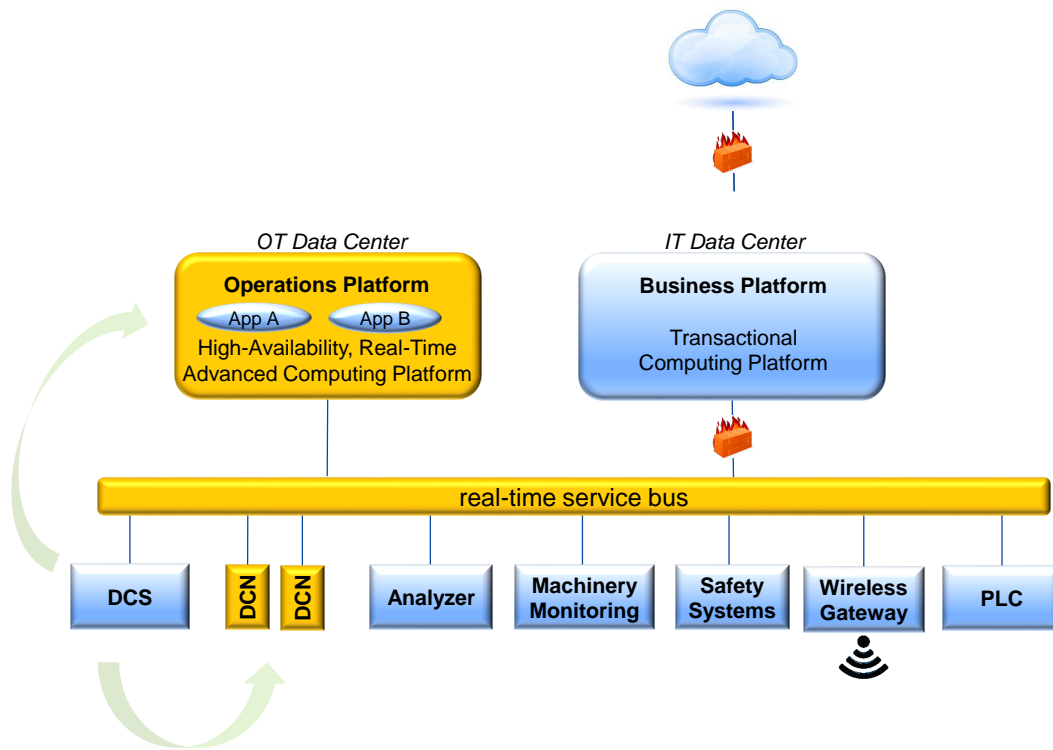
Segment	1 Comp		2 Comp			L
	G	GLN	G-G	G-GLN	GLN-GLN	
1H	20	39	13	14	7	7
4H	23	36	11	10	6	14
16H	30	42	7	4	4	13

TABLE 2. Empirical probabilities computed using (1) where $o_{i,j}$ is the element in the i th row and the j th column. The background colors highlight the block diagonal structure of the matrix which implies that the nodes belong to two distinct groups, where the nodes within the same group often were in the same fading state.

$\%$	\mathbf{x}_1	\mathbf{x}_2	\mathbf{x}_3	\mathbf{x}_4	\mathbf{x}_5	\mathbf{x}_6
\mathbf{x}_1	.	0.74	0.90	0.79	0.17	0.14
\mathbf{x}_2	0.96	.	0.96	0.95	0.16	0.14
\mathbf{x}_3	0.67	0.55	.	0.75	0.16	0.14
\mathbf{x}_4	0.75	0.68	0.95	.	0.15	0.12
\mathbf{x}_5	0.23	0.17	0.29	0.22	.	0.7
\mathbf{x}_6	0.28	0.21	0.3	0.25	0.99	.

TABLE 3. Step response performances of three sampling schemes for the reject tank: Fast periodic $h = 0.5$ [s] (FP), slow periodic $h = 5$ [s] (SP), and event-based $\bar{e} = 0.5$ (EB). Performance is evaluated through communication reduction (CR) and the three measures integrated absolute control error (IAE), integrated squared control error (ISE), and over-shoot (OS).

Scheme	CR	$\int e(t) $	$\int e(t) ^2$	OS
FP	0%	141.3	295.9	15.0%
SP	90.0%	229.7	486.2	53.7%
EB	87.9%	174.9	392.1	22.5%



1

Figure 1. Layout of a future control architecture (with ExxonMobil’s permission): The system contains distributed control nodes, used as dedicated single-channel I/O modules, with control capability. Through a real-time data service bus, they are connected to the operations open platform running open-source software. This setup together with a common “app” platform is expected to replace the traditional automation pyramid, which structurally separates process control, scheduling and planning to their own hierarchical levels; leading to a more flexible and cost effective paradigm.



Figure 2. The Iggesund paper mill, which is part of Holmen group, is in Iggesund. The small community in Iggesund is located on the coast of the Bothnian Sea, Sweden's east coast. The mill produces one of the world's leading paperboard brand, Invercote. About 700 people work in Iggesund paper mill and the factory produces about 420,000 tons of pulp and about 330,000 tons of cardboard every year.



Figure 3. Iggesund's paper mill has two paper machines of the kind mentioned above. The machines are 300 m long and produce state-of-the-art cardboard. The photo is taken from the wet end of the cardboard machine 2. At the far right of the picture is the wire section where the pulp comes out of the headboxes and is dewatered on the wire. The pulp then contains more than 99% water. To the left of the picture you see the drying unit where the cardboard is dried by steam.

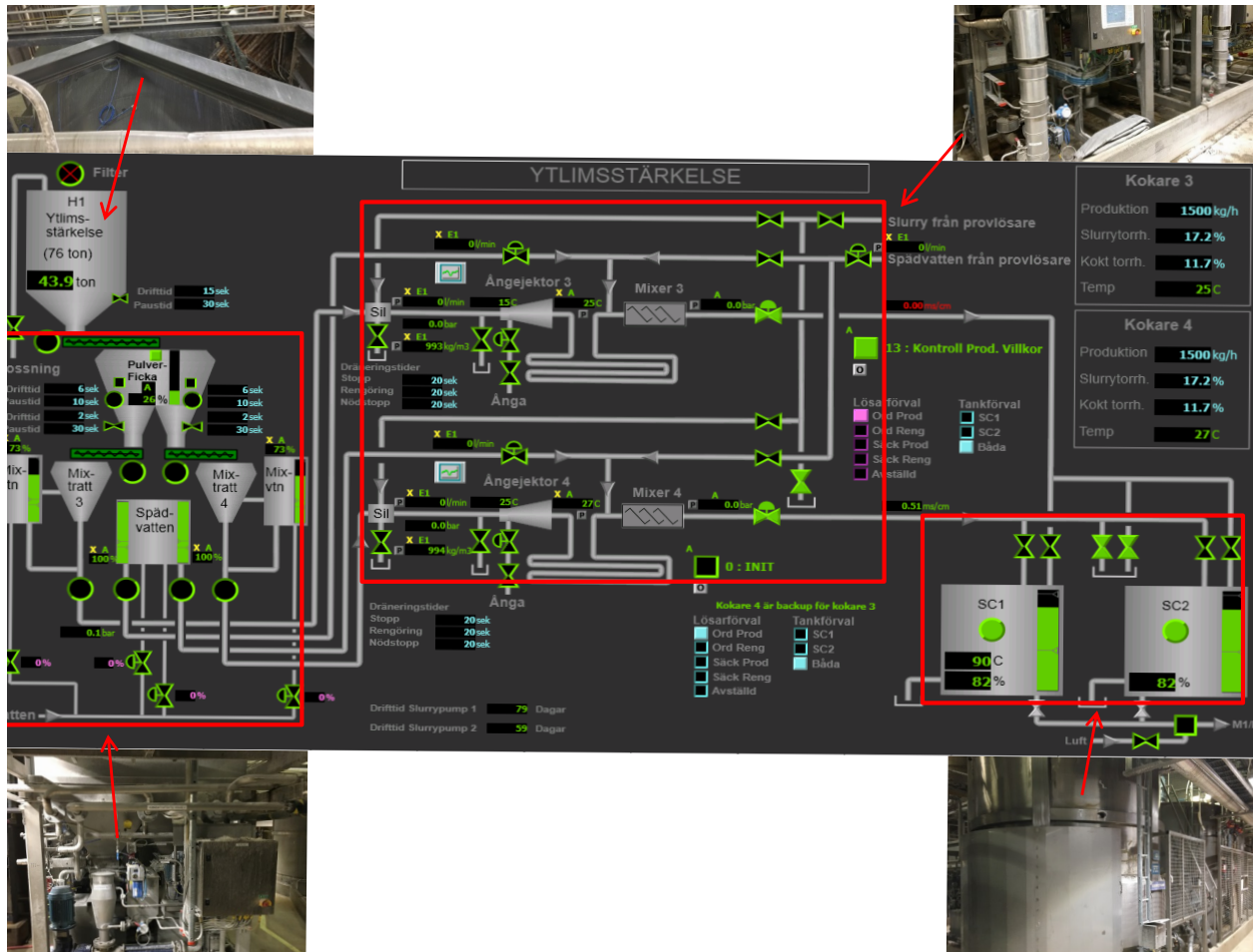


Figure 4. The starch cooker process illustrated by the operator panel in the middle and photos of the real process equipment in the corners above and below the operator panel. Top left: Starch powder buffer. Top right: Starch boiler. Bottom left: Mixing tank for starch powder and water. Bottom right: Storage tank for boiled starch. The red arrows relate the respective process equipment to the operator panel.

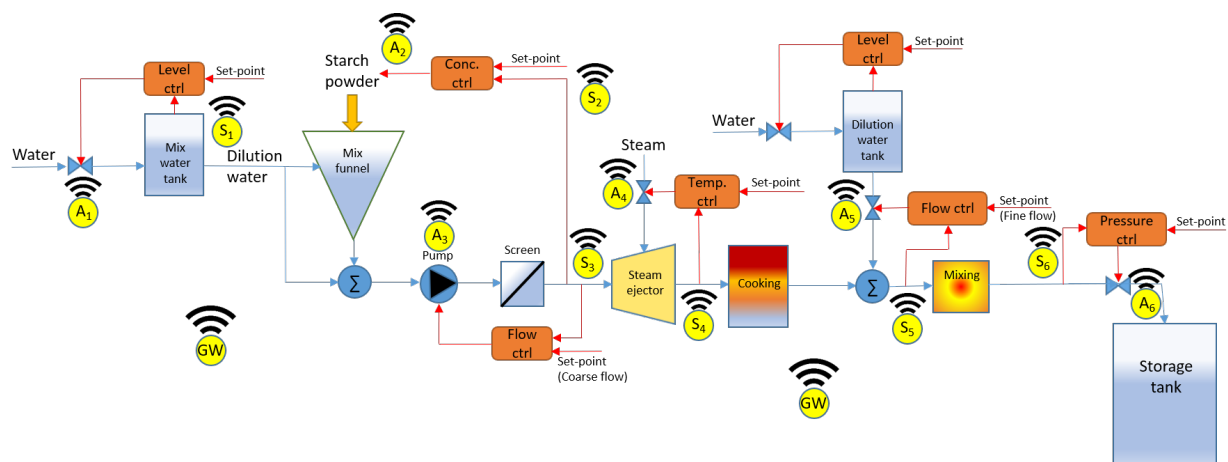
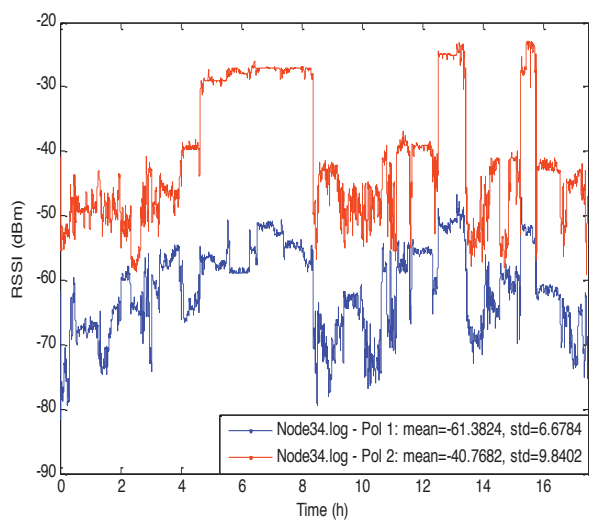
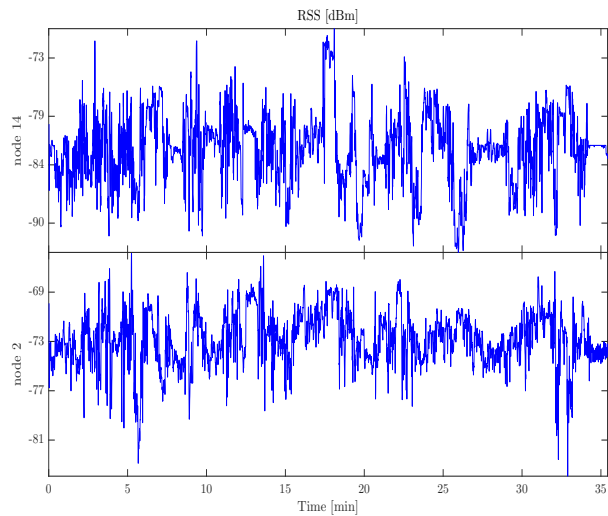


Figure 5. Block diagram of the Iggesund Paperboard starch cooker, also illustrated in the operators panel of Figure 4. The process starts with filling a water tank (depicted at the top left of the figure), from which water is used to mix with the starch in a mixing funnel. In order to remove lumps of starch, the mixture is pumped through a screen before steam is injected for cooking. In order to finely adjust the starch concentration after cooking, small amounts of dilution water might be added before storing the product in a storage tank (see the bottom right corner of the figure). The architecture, consists of multiple wireless feedback loops involving sensors (S_j) and actuators (A_j) to control each step of the process.



(a)



(b)

Figure 6. Channel gain variability between two sensor nodes located next to the paper machine finish line at Iggesund Paperboard paper mill. The crane in the ceiling moving around the paper rolls causes the gain variability, (a) vertical polarization (red), horizontal polarization (blue), and channel gain variability realizations between two pairs of sensor nodes in the starch cooker section. The variability is primarily caused by people moving in the environment of the sensor nodes, (b).

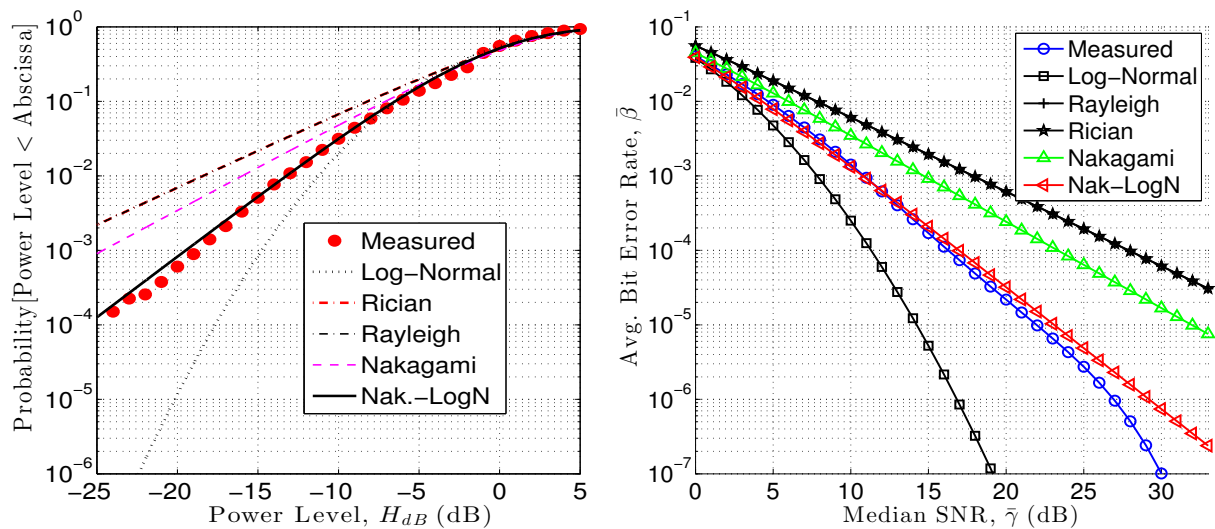


(a)



(b)

Figure 7. Iggesund Paperboard paper mill. (a) Channel measurement between two nodes located on opposite sides of the aisle next to the paper mill finish line in Iggesund. A typical channel gain variability is depicted in Figure 6 a. The green dots indicate the approximate positions of the sensor nodes. (b) Aisle in the cooker environment where wireless sensor nodes were deployed. Typical channel gain variabilities between pairs of nodes are depicted in Figure 6 b.



(a) Estimated and empirical cumulative power level distributions (in dB) based on all measured links over 17 hours.

(b) Theoretical and empirical average bit error rate (BER) as a function of the median signal to noise ratio (SNR) based on all measured links over 17 hours.

Figure 8. Theoretical and empirical evaluations taken over all wireless link data acquired during a measurement campaign at Iggesund Paperboard, Sweden during 17 hours. The diagrams above are from [15] and republished here with the consent of IEEE.

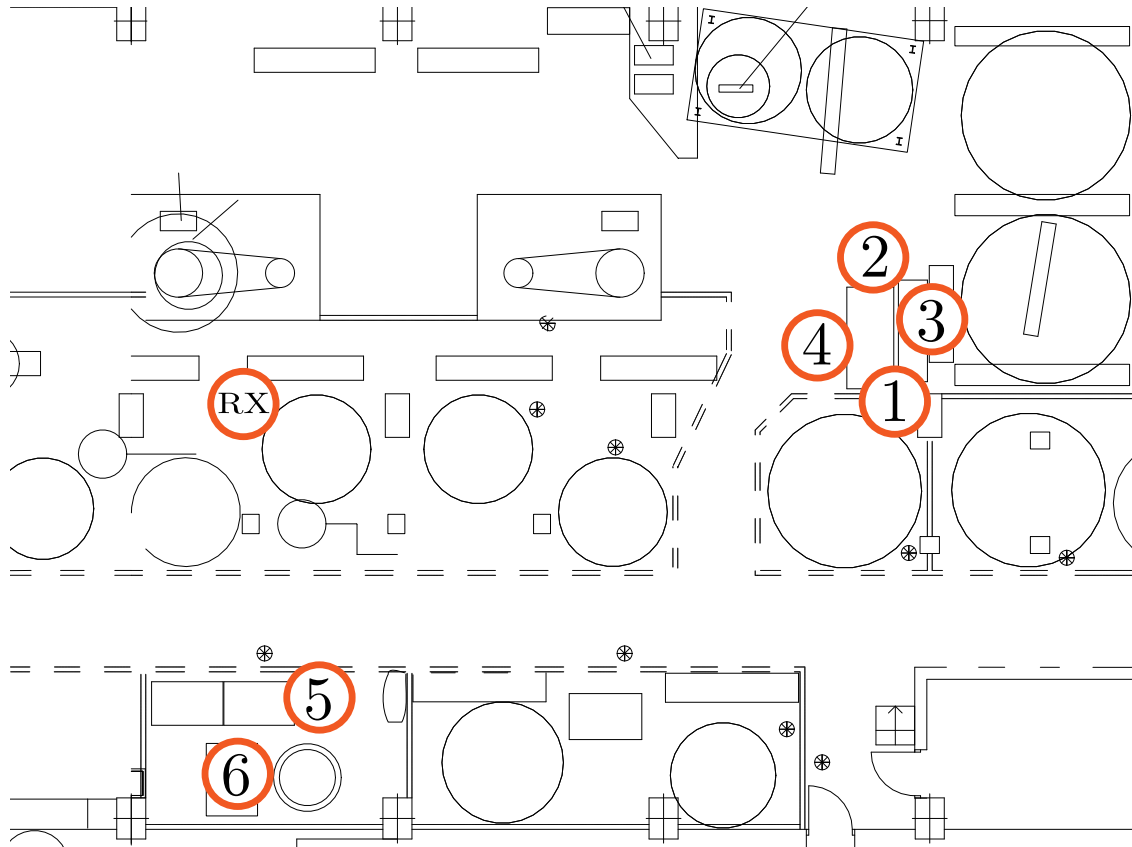


Figure 9. Overview of the deployment area at the paper mill in Iggesund. The circles indicate the positions of the wireless sensor nodes which were deployed in close proximity to machines to mimic a realistic wireless control scenario.

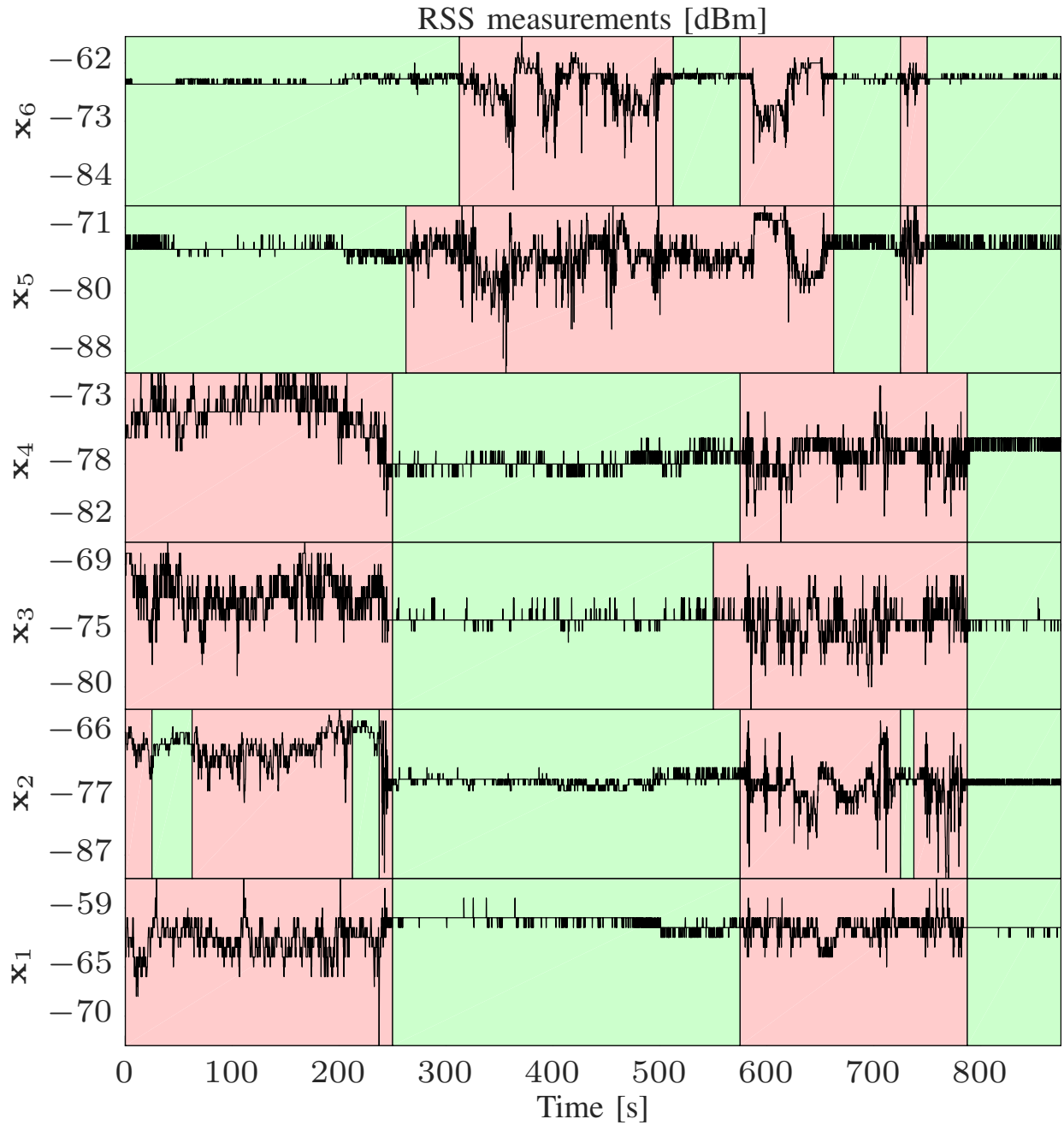
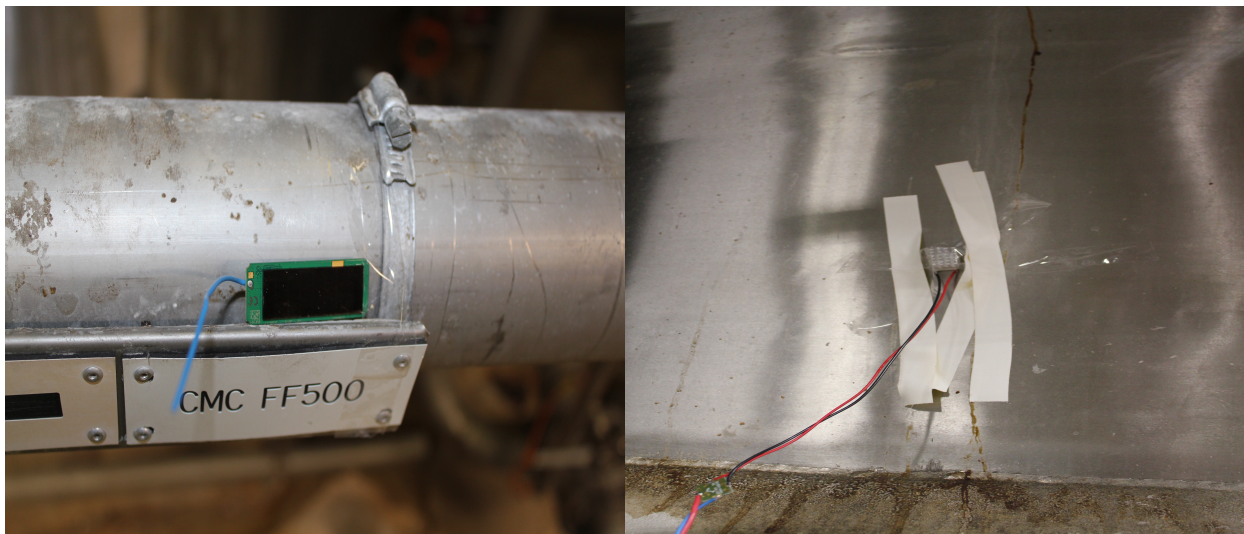


Figure 10. Time series of recorded received signal strength (RSS) for the network in Figure 9. The green and red fields mark the estimated periods of quiescent and volatile fading, that is, where $\hat{z}_{l,t} = 0$ and $\hat{z}_{l,t} = 1$, respectively. Since the nodes x_1 - x_4 were positioned relatively close to each other, we see that they often were in the same fading state. As expected, nodes x_5 and x_6 exhibited similar behavior.



(a) Wireless sensor, powered by solar cell.

(b) Peltier element at hot tank.

Figure 11. Energy harvesting devices used for experiments at Iggesund paper mill. (a) Small wireless sensors with solar cells were used to harvest energy from the factory lighting. (b) Also, Peltier elements were located at several hot surfaces (for example pipes and tanks) to harvest energy from the temperature gradient.

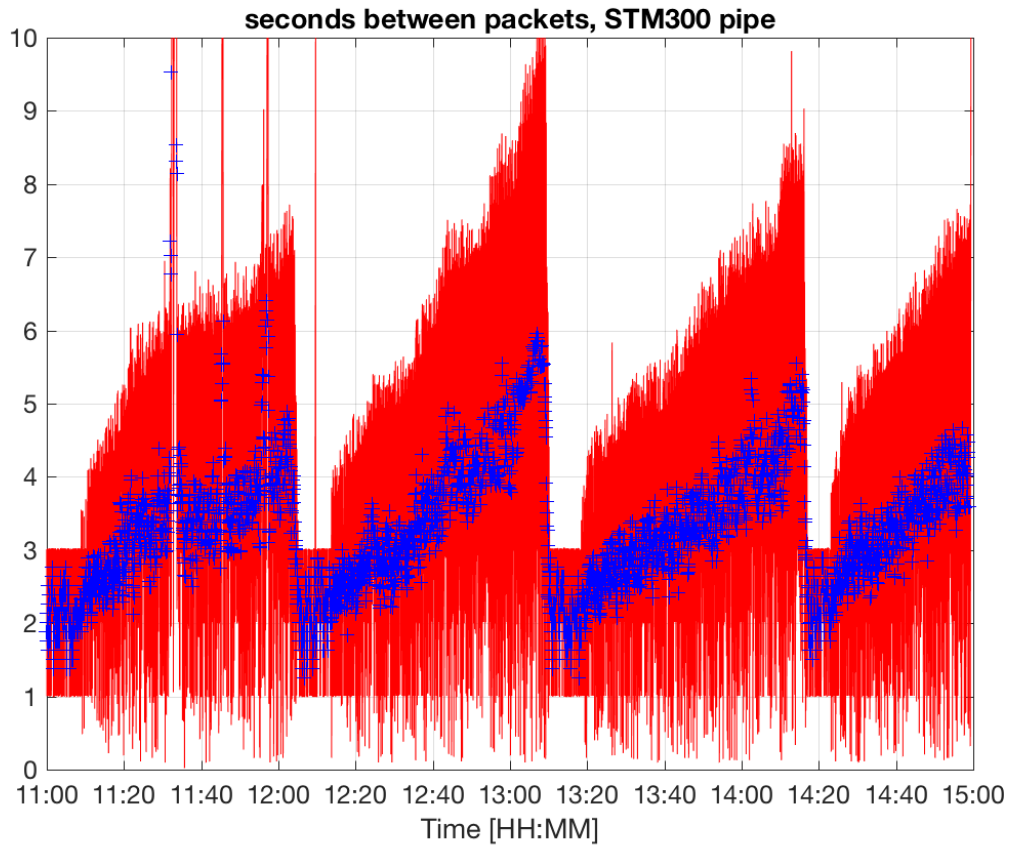


Figure 12. Time between consecutive packets received from a wireless sensor at node 4 powered by a Peltier element attached to a hot pipe; raw data (red) and filtered (blue). It is clearly visible, that the time between two consecutive packets changes periodically. This is due to the harvested energy that is used to send the packets also changes periodically. Indeed, the pipe, at which the Peltier element was located, transports hot liquids to a batch process. This takes a few minutes, in which the pipe gets very hot. Afterwards, the temperature decreases slowly, so that the harvested energy also slowly decreases and the time between the packets increases. The batch process is then repeated roughly every hour so that the patterns repeat periodically.

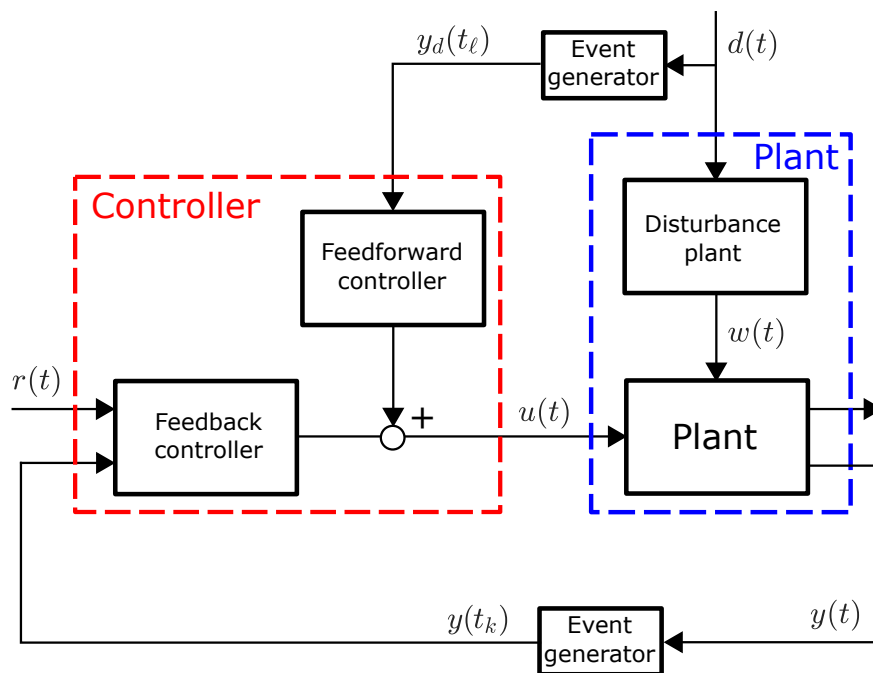


Figure 13. Block diagram of event-based feedback and feedforward control. The red box indicates the controller. The feedforward controller adjusts the control signal from the feedback controller based on the information from the disturbance sensor. The blue box indicates the plant which consists of the disturbance plant and main plant. Event generators are introduced at the plant and disturbance sensors. Transmission events are generated if the sensor measurements change significantly.

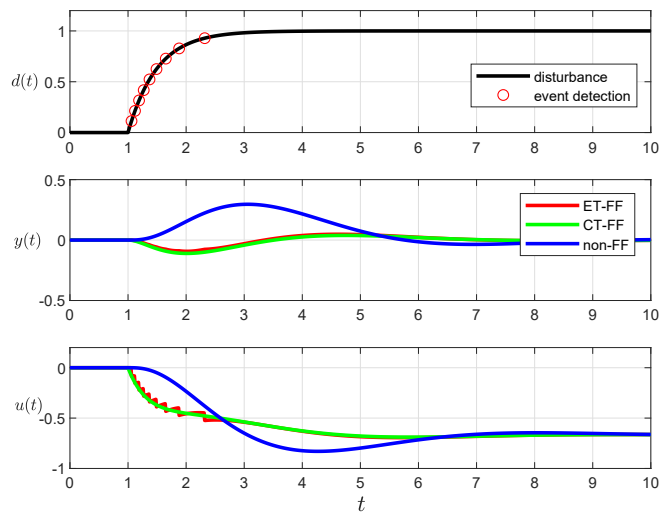


Figure 14. Simulations of disturbance responses. Top: Disturbance and event generation times. Middle: Outputs of three cases; (i) with event-based feedforward control (red, ET-FF), (ii) with continuous-time feedforward control (green, CT-FF), and (iii) no feedforward control (blue, no-FF). Bottom: Inputs of the same three cases. The simulations show that the event-based feedforward control performs equally well to the continuous-time feedforward control with only nine transmissions of the disturbance measurements. See [20] for more details.

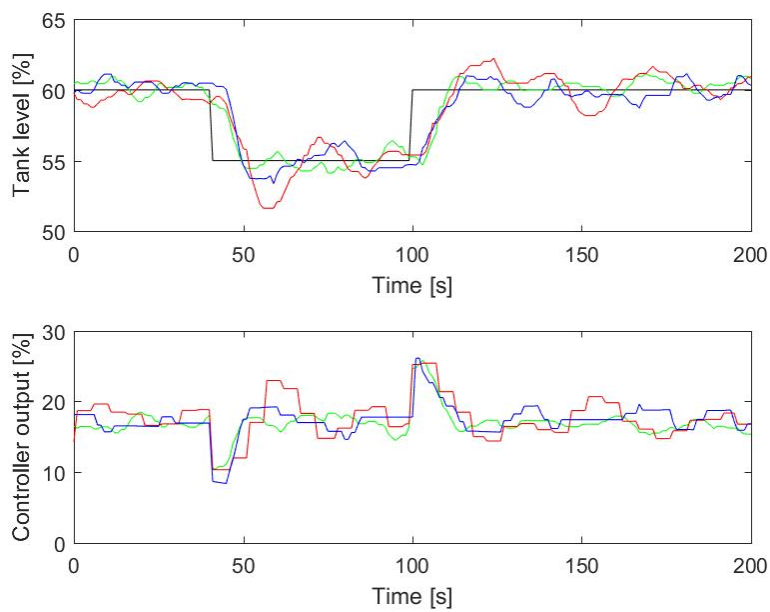


Figure 15. Step responses on the reject tank process at Iggesund for three sampling schemes: Fast periodic $h = 0.5$ [s] (green), slow periodic, $h = 5$ [s] (red), event-based $\bar{e} = 0.5$ [s] (blue) control. The event-based control still has similar performance compared to fast periodic despite almost 90% communication reduction. See also Table 3.

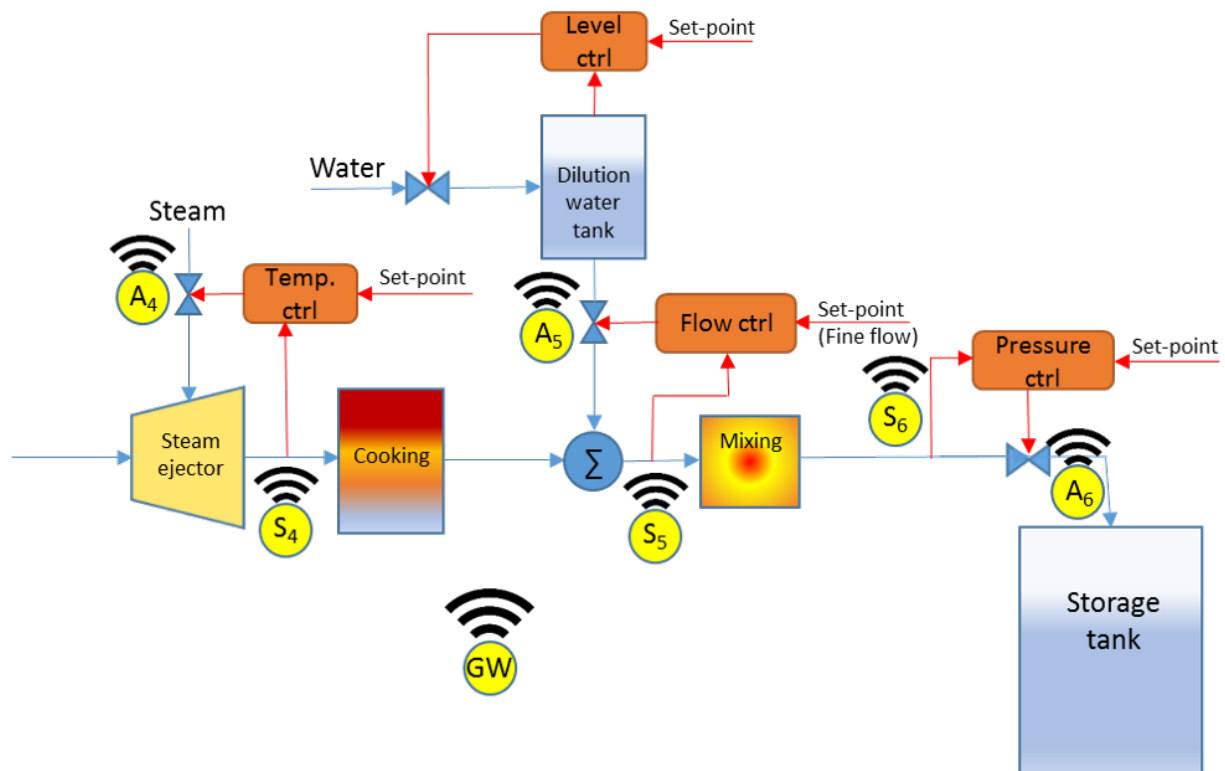


Figure 16. Block diagram of a starch cooker. Three control loops are installed with wireless actuators and wireless sensors. The level controller is a PI controller, the temperature controller is also a PI controller, and the pressure controller is a PID controller.



Figure 17. The environment where the wireless devices were installed. The picture shows a mixing tank where the flow of the slurry into the cooking process is measured. The gateway and the field devices were realized by assembling two off-the-shelf evaluation boards in an IP67 enclosure. A CAN bus IO from ABB (CI581) with analogue inputs and outputs, as well as digital counterparts, was connected to the field devices.

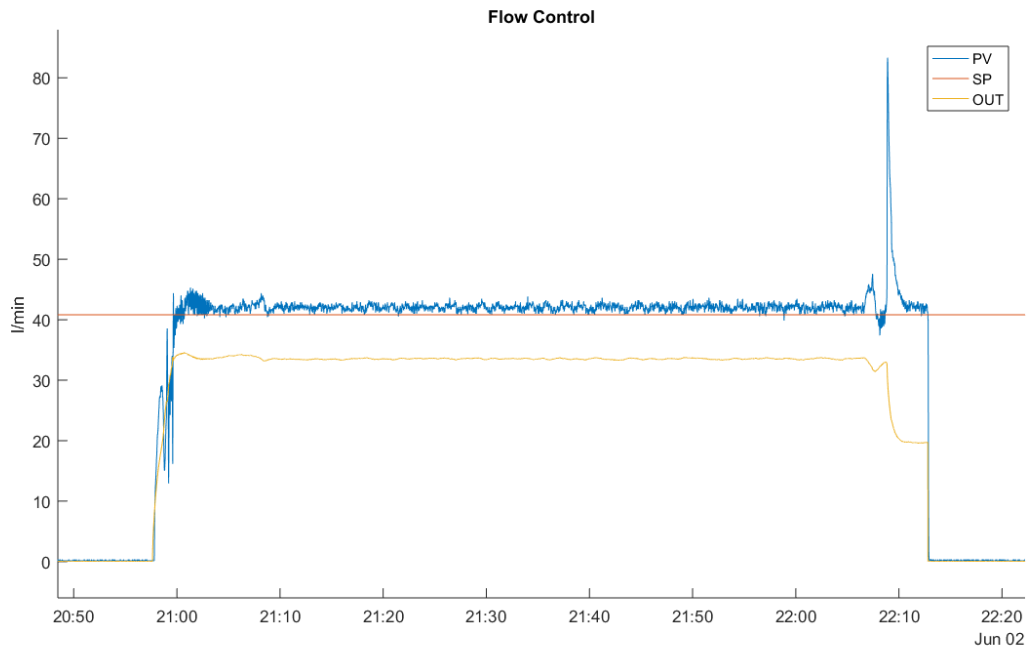


Figure 18. Performance of the flow controller during the starch cooking process. PV is the process value in l/min, SP is the set-point, and OUT is the output signal to the control valve in %. At the beginning of the batch sequence at 21:00, the flow controller aims to keep a water flow of 41 liters/minute. Shortly before 22:10, the level of the storage tank has reached the upper threshold such that the control valves to the storage tanks are closed and a cleaning process starts. The opening of the pressure valve (see also Figure 19) for cleaning acts as a flow disturbance. The cleaning process finished at 22:15 and the starch cooking system is ready for another batch as soon as the storage tank level reaches its lower threshold.

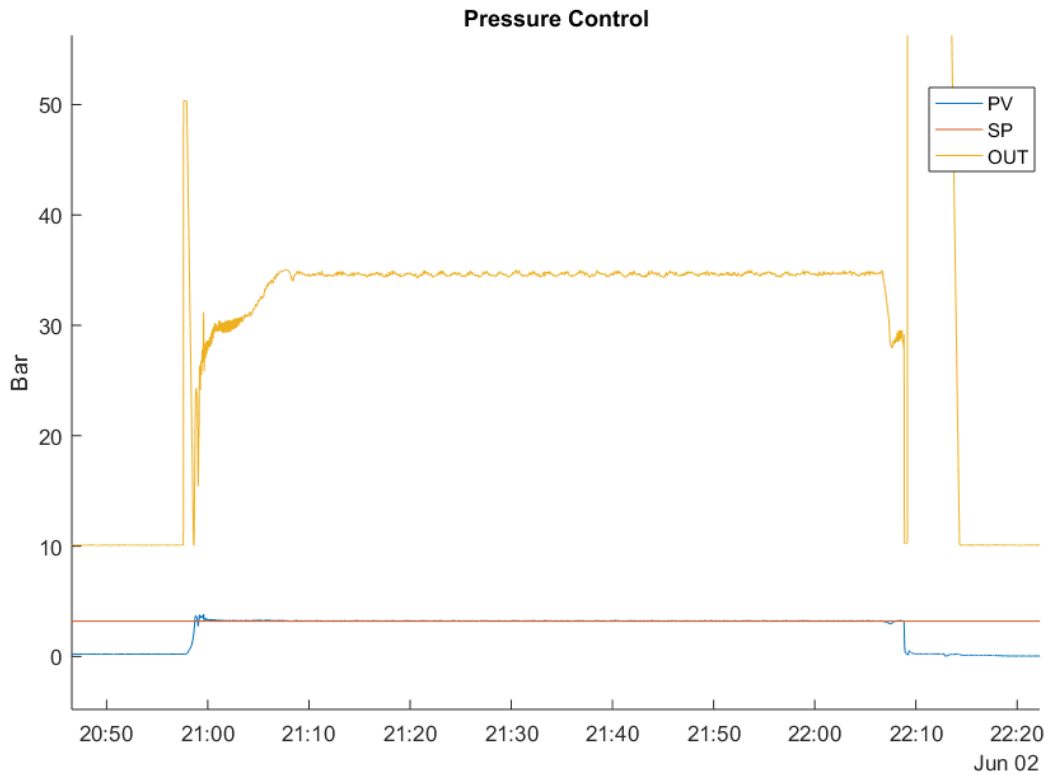


Figure 19. Performance of the pressure controller during the starch cooking process. PV is the process value in Bar, SP is the set-point, and OUT is the output signal to the control valve in %. At the beginning of the batch process at 21:00, the control valve of the pressure controller is opened to 50% to flush out remainders of starch from the previous batch. Then, the pressure controller aims to maintain a pressure of 3.3 Bar while heating the boiler (see Figure 20). Once the batch process is completed just before 22:10, the cleaning process starts by opening the pressure valve and finishes at 22:15.

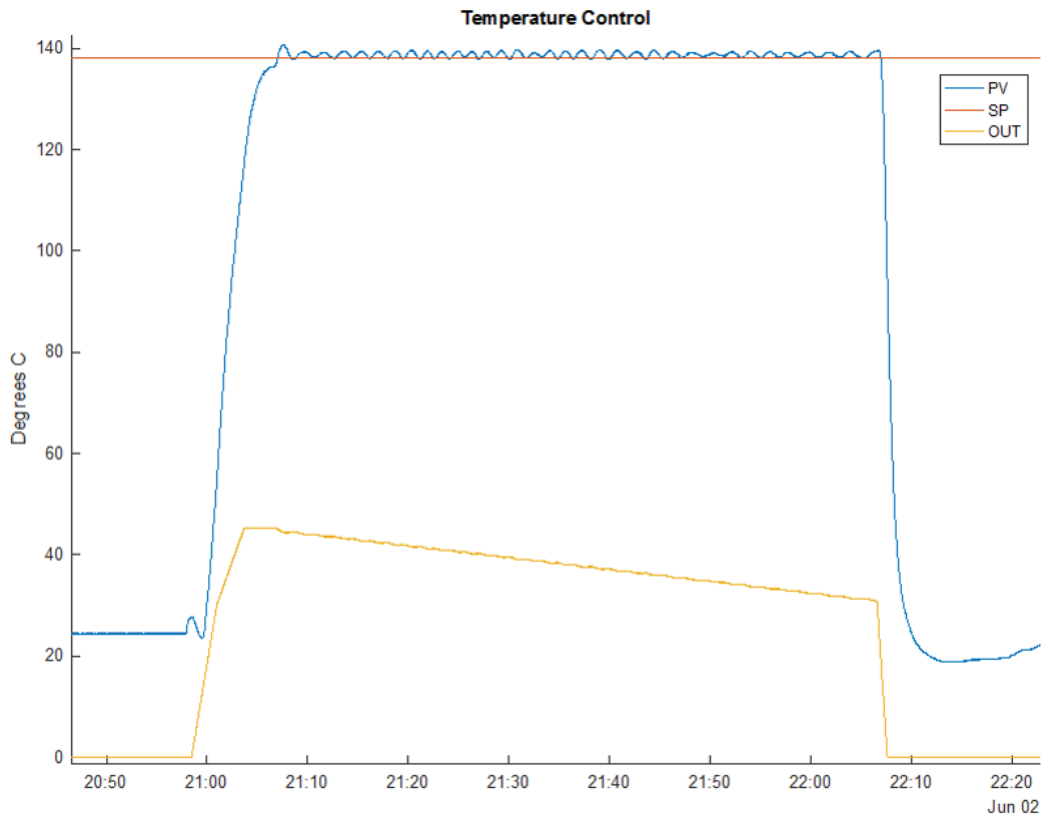


Figure 20. Performance of the temperature controller during the starch cooking process. PV is the process value in Celsius, SP is the set-point, and OUT is the output signal to the control valve in %. At the beginning of the batch process around 21:00, the boiler starts to heat with steam using a ramp in the output of the control valve. When reaching the desired temperature of 138 degrees Celsius shortly after 21:00, the temperature controller is enabled to maintain the temperature.

Sidebar: Summary

2 Wireless sensor networks are to a growing extent being deployed in process industry,
but there are still several issues that need to be addressed for this technology to reach its
4 full potential. This paper describes some of the main challenges in next generation process
control, with an architecture based on distributed control nodes connected to a real-time data
6 bus over wireless and wired networks. A case study focused on one of the starch cooker
processes of the Iggesund pulp and paperboard mill in Sweden is used to illustrate various
8 challenges and solutions to sensing, communication, and control for emerging wireless process
automation. Radio environment modeling, network protocol design, energy harvesting, and event-
10 based control are discussed in some detail. Experimental tests on the starch cooker during normal
production over five consecutive days indicates that it is sometimes possible to replace wired
12 control systems with wireless in complex industrial environments.

Sidebar: Iggesund Mill History

2 Iggesund Mill's origin is found in the forests outside Hudiksvall in Sweden, more
specifically in the small town of Iggesund. The society has a long history, already in the middle
4 of the 16th century there were small industries in and around the town. In 1685 the trader and
chief commissioner, Isak Breant, received a license to construct an ironworks in the lower part
6 of Iggesundån (Iggesund River). Soon thereafter the production was started at the plant.

However, in the upper part of Iggesundån there was already a paper mill, Östanå paper
8 mill. Iggesund Mill bought this paper mill in 1771. The Östanå paper mill was the first in the
world to try to produce paper from sawdust and wood, but the experiments never reached beyond
10 the experimental stage and in 1842 the paper mill burnt down.

In 1869, Baron Gustav Tamm took over as owner of Iggesund Mill and he was able to
12 construct a large sawmill which he started to build in 1870. In addition to the purchase of Östanå
paper mill, this marks the first transition from a refined iron industry to a wood industry. Between
14 the years 1915-1917, a cellulose factory was built on a new site further away from Iggesundån.
For a photo from 1916, see Figure S1. In 2017, the company celebrated that the factory had
16 been 100 years in the same location as today.

Today, Iggesund Mill is best known for its white premium cardboard, but it was not until
18 the beginning of the 1960s that they started making cardboard at the mill. Iggesund Mill was
only the third manufacturer in the world which installed a carton machine with the new modern
20 technology; the other two were previously in Australia and England. In 1963 the first cardboard
machine at the Iggesund Mill was started. The second cardboard machine was started in 1971.

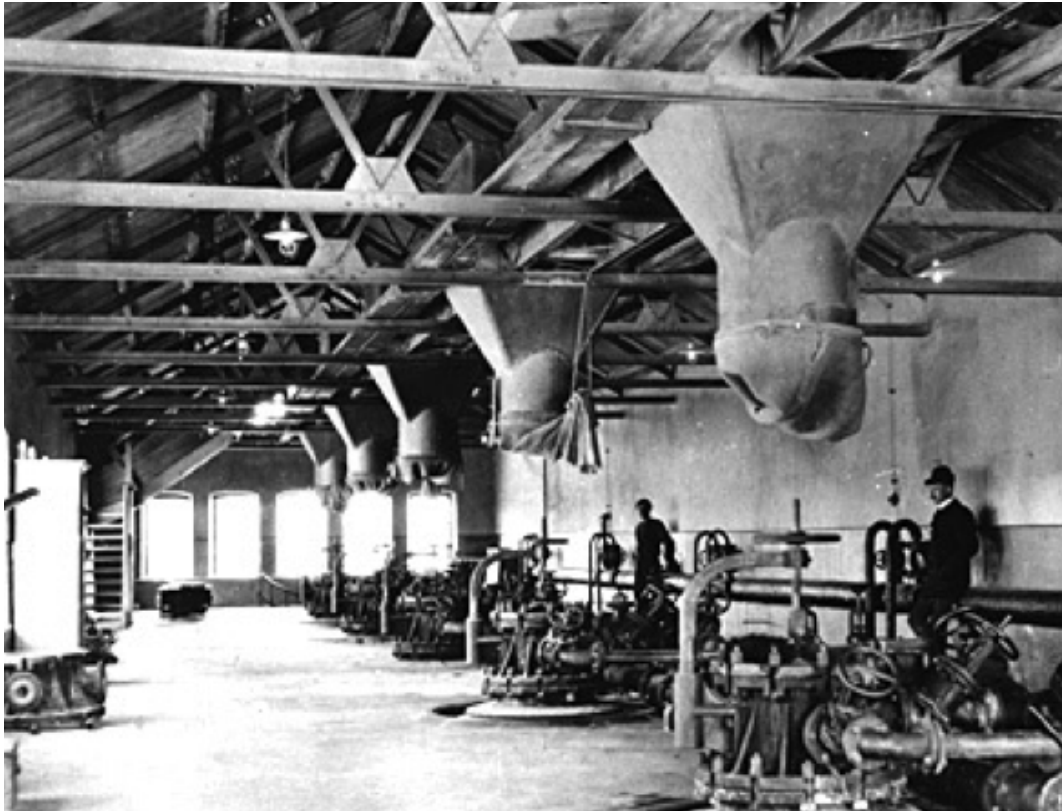


Figure S1. The photo is taken in the production room of the old sulphite digester. The house has long been demolished and today there are no traces left of it. At that time when the photo was taken 1916, the sulphite process was used to produce pulp. Today, the process has changed and instead it uses the sulphate process to achieve a better quality and whiteness of the pulp.



Figure S2. Aerial view of Iggesund Bruk from 1940. At that time, Iggesund Bruk was only a pulp mill. The first cardboard machine was started in 1963 and with this Iggesund Bruk became both a producer of pulp and cardboard. The factory area is still in the same location as when the first pulp mill started in 1916.



Figure S3. Iggesund Paperboard's first cardboard machine called KM1 and is still in use, but since the photo was taken in 1968, it has been rebuilt several times. The photo is taken so that you see the reeling of the cardboard and in the middle of the picture you see the coating stations. At the far left of the picture, the drying unit of the cardboard machine is visible.

Sidebar: Radio Model Selection

2 Radio links of the kind depicted in Figure 6 can be modeled as a mixture probability density function (pdf) with M components,

$$p(y|\varphi) = \sum_{i=1}^M P_i p(y|\theta_i), \quad (\text{S1})$$

4 where y is the underlying continuous variable representing power, P_1, \dots, P_M are mixture probabilities satisfying $\sum_i P_i = 1$, and $p(y|\theta_i)$ is the pdf of the i :th mixture component that
6 is described by the parameter vector θ_i , and $\varphi = \{\theta_1, \dots, \theta_M, P_1, \dots, P_M\}$.

The corresponding discrete distribution for quantized data is obtained by integration over
8 the user selected bin intervals, say $I_k, \forall k$, that is,

$$P(k|\varphi) \triangleq Pr(y \in I_k|\varphi) = \int_{y \in I_k} p(y|\varphi) dy \quad ; \quad \forall k. \quad (\text{S2})$$

As will be explained below, see also Figure 8, an individual mixture component, $p(y|\theta_i)$,
10 is preferably modeled as either purely Gamma (G), log-Normal (LN), or Gamma log-Normal (GLN) distributed. The G distribution in the power domain is given by

$$p_G(y) = \frac{m^m \exp\left(m \frac{y-\bar{y}}{\mu}\right) \exp\left(-m \exp\left(\frac{y-\bar{y}}{\mu}\right)\right)}{\mu \Gamma(m)}, \quad (\text{S3})$$

12 where \bar{y} is the mean, μ is a constant, and m is the Nakagami- m parameter. Hence, the pure G component can be parameterized by $\theta_i = (\bar{y}_i, m_i)$.

14 The compound GLN fading model arises for a power gain that is the product of two independent factors where one is G distributed and one is LN distributed. Expressed in dB, the
16 LN distribution is

$$p_{LN}(y) = \frac{1}{(2\pi)^{1/2} \sigma} \exp\left(-\frac{y^2}{2\sigma^2}\right) \quad (\text{S4})$$

where σ is the standard deviation and where we, without loss of generality, have set the mean to
18 zero. Expressed in y , the above mentioned product becomes a sum of independent variables and the resulting pdf for this sum, $p_{GLN}(y)$, is given by the convolution $p_{GLN}(y) = p_G(y) * p_{LN}(y)$.
20 The GLN component is thus parameterized by the tuple $\theta_i = (\bar{y}_i, m_i, \sigma_i)$.

Sidebar: Data Generation Model

Let $\mathbf{x}_l = [x_{l,1}, \dots, x_{l,T}]$ denote T scalar Received Signal Strength (RSS) measurements from the l th link. The observations in \mathbf{x}_l are assumed to be generated by a two state Hidden Markov Model (HMM), where $z_{l,t} \in [0, 1]$ denote the state of the model that is associated with the l th time series at time t . As described in more detail below, $z_{l,t}$ parameterizes the generative distribution of $x_{l,t}$. The state sequence $\mathbf{z}_l = [z_{l,1}, \dots, z_{l,T}]$ is generated by a Markov model with transition probabilities, $Q_l = \{q_{l,i,j} : i, j \in [1, 2]\}$, where $q_{l,i,j}$ denotes the probability,

$$q_{l,i,j} = P(z_{l,t+1} = j | z_{l,t} = i). \quad (\text{S5})$$

The initial state distribution is denoted $\boldsymbol{\pi}_l = \{\pi_{l,i} : i \in [1, 2]\}$ where,

$$\pi_{l,i} = P(z_{l,1} = i). \quad (\text{S6})$$

Each state generates observations from an AR process, such that

$$x_{l,t} = \mathbf{x}_{l,t-1:t-v} \mathbf{a}'_{l,z_{l,t}} + e_{l,t}, \quad (\text{S7})$$

where $\mathbf{a}_{l,z} = [a_{l,z,1}, \dots, a_{l,z,v}]$ are the AR-coefficients for state z , v is the order of the process, and $e_{l,t}$ is independent, zero-mean, Gaussian noise with variance σ_{l,z_t}^2 .

We choose to label the states so that state $z_{l,t} = 1$ corresponds to the more volatile fading state, for example, $\sigma_{l,1}^2 > \sigma_{l,0}^2$. Also, we fix $v = 2$ which results in a satisfactory segmentation performance for all time series. Let $\Lambda_l = \{Q_l, \boldsymbol{\pi}_l, \mathbf{a}_l, \boldsymbol{\sigma}_l\}$ denote the collection of model parameters where $\mathbf{a}_l = \{\mathbf{a}_{l,z} : z \in [1, 2]\}$ and $\boldsymbol{\sigma}_l = \{\sigma_{l,z}^2 : z \in [1, 2]\}$.

Estimation of model parameters

In [18], Rabiner outlined an iterative algorithm for computing the maximum likelihood estimate, $\hat{\Lambda}_l$, of the model parameters,

$$\hat{\Lambda}_l = \arg \max_{\Lambda_l} P(\mathbf{x}_l | \Lambda_l), \quad (\text{S8})$$

and we refer the interested reader to the original work for details on the algorithm.

Since the inference objective is to use the HMM to detect changes in volatility, the RSS measurements were preprocessed with a bandpass filter with cutoff frequencies at $[\frac{1}{2}, 2]$ Hz. This eliminated slow varying trends and measurement noise from \mathbf{x}_l prior to estimation of $\hat{\Lambda}_l$.

Inference of the state sequence

2 Conditioned on $\hat{\Lambda}_l$, the most likely state sequence, $\hat{\mathbf{z}}_l = [\hat{z}_{l,1}, \dots, \hat{z}_{l,T}]$, is obtained by maximizing,

$$\hat{\mathbf{z}}_l = \arg \max_{\mathbf{z}_l} P(\mathbf{x}_l, \mathbf{z}_l | \hat{\Lambda}_l), \quad (\text{S9})$$

4 and the solution can be computed using the Viterbi algorithm in [18].

Sidebar: Advances in Wireless Control

2 Along the development of wireless technology, industrial control by means of wireless
communications has received much attention in both academia and industry. Recent research
4 issues on control over wireless communications, especially in industrial automation systems,
are summarized in [2], [5], [9], [S1]–[S4]. In [5], [S1], [S2], some communication protocols
6 developed for industrial wireless communications such as WirelessHART [S5] and ISA-100 [S6]
are discussed. In both WirelessHART and ISA-100, their hardware and protocols are specified by
8 the standard of the low rate wireless personal area network, IEEE 802.15.4 [S7]. Some research
focus on the implementation and design of control systems operating over the WirelessHART and
10 ISA-100 communication protocols. In [S8], aperiodic control algorithms implemented over the
IEEE 802.15.4 standard are proposed and evaluated on a double-tank laboratory experimental
12 set-up. A network model which captures some important key aspects of the WirelessHART
protocol – a multi-hop structure and TDMA communications with some different frequencies –
14 is developed in [S9], [S10]. Emulation-based stability conditions are derived in [S9] and observer
design under the impact of stochastic noise is discussed in [S10]. A model of control systems
16 over a multi-hop network is proposed in [S11]. Based on this model, a co-design framework
comprising both controller and network scheduling and routing is investigated in [S12]. In [S13],
18 a co-design of LQG control and multi-hop network scheduling and routing and its reconfiguration
is discussed. In [S14], a co-design of controller and network scheduling and routing is proposed
20 for the WirelessHART standard, which is assumed to have network reconfiguration after a given
period.

22 Wireless control is also studied in the context of networked control theory, which in general
focuses on control problems under network-induced constraints such as delay, packet dropout,
24 and channel capacity limitation [4], [S15]–[S17]. In [S18], LQG control with packet dropouts
is considered. In [S19], a network with multiple sensors is considered while communication
26 through intermediate nodes is studied in [S20]. LQG control with network induced delays and
access constraints is investigated in [S21], [S22] where only a subset of sensors can access the
28 controller. Network capacity is explicitly considered as a control theory- and information theory
problem in [S23]–[S25].

30 Scheduling of data transmission of networked control systems has attracted attention to
reduce the amount of communication. In [S26], [S27], a joint optimization problem is presented
32 where the problem can be separated into an optimal estimation, an optimal control, and an optimal
scheduling problem. Scheduling among multiple control loops with a shared communication
34 network is proposed in [S28], [S29]. A prioritizing framework under limited channel slots is
proposed in [S28], and a scheduling framework under a Media Access Control (MAC)-like

protocol is developed in [S29]. There is a lot of research considering sensor scheduling for state
2 estimation. In [S30], a communication control scheme for Kalman filters is developed to improve
the trade-off between estimation performance and communication cost. Optimal estimation with
4 a multiple time-step cost is introduced in [S31]. The minimum mean square error (MMSE)
estimation schedule can be obtained in some special cases. In [S32], the MMSE schedule between
6 two sensors is obtained, which is extended to more sensors in [S33], [S34]. These works deal with
a single-hop network, that is, every sensor can directly communicate with the remote estimator.
8 A multi-hop network structure is considered in [S35]–[S37]. In [S36], [S37], the authors consider
how to manage the control systems when the network environment is changed. In [S36], they
10 propose a way to reconfigure the network under time-varying channel states.

Energy-aware control strategies over wireless communication is investigated in some
12 previous work. Optimal sensor energy allocation is studied in [S38]–[S40]. Therein, the energy
consumption is dealt with as a control variable, which determines the probability of packet loss.
14 Energy allocation for state estimation is discussed in [S38], [S40]–[S42] and for optimal control
in [S39]. Network control systems with energy harvesting sensors are considered in [S43]–[S45].

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2 **Sidebar: Advances in Event-based Control**

Event-based sampling for the classical feedback control loop has been studied, often as a means to reduce communications among the system components without sacrificing performance, see, for example, [S46]–[S48], and the references therein.

Optimal estimation and LQG control with event-based sampling strategies are discussed by many researchers. The authors of [S49] offer a deterministic event-based scheduler by using feedback from the estimator. A stochastic schedule is proposed in [S50]. With a similar setup, a scheduling framework where the transmissions are invoked by the estimation error covariance is proposed in [S51]. In [S52], packet dropouts are considered for covariance-based state estimation. These works are then extended to LQG control problems in [S53]. In [S54], a TDMA-like time-triggered schedule as well as a CSMA-like event-triggered schedule with random or dynamic scheduler are analyzed. Multi-hop networks are explicitly considered in some studies. LQG control with event-based sampling is investigated in [S27], where an optimal design of the controller and the event-triggering law is obtained. The trade-off between LQG control performance and communication load for stochastic event-based control is discussed in [S55]. LQG control where the event-based communication is performed over WiFi is considered in [S56].

To implement event-based control strategies into industrial control loops, event-based PID control has been considered, for example, in [21], [22], [27], [S57]–[S60]. The works include both academic and industrial perspectives. As presented in [21], event-based PID control can significantly reduce the communication effort with only a slight or no degradation in control performance, which has motivated the process industry to use event-based PID control [28]. In [24], [25], event-based PID control is evaluated at an industrial paper mill plant in Iggesund. Some practical problems when introducing event-based PI control are discussed in [26], [27], [S59]. In [27], it is shown that event-based sampling may result in a sticking effect or stationary large oscillations. To overcome these problems, [27] proposes PIDPLUS [S61]–[S63]. The asymptotic stability conditions are derived with a relative threshold policy in [S59]. Furthermore, [26], [S60], [S64], [S65] focus on actuator saturation for event-based control. In fact, the stability region is influenced by the use of event-based control. In [26], it is shown that an anti-windup technique can significantly improve the performance for event-based control systems saturation. The authors of [S65] introduce an event-based anti-windup scheme. In [S60], the authors consider a zero-order hold between the controller and the actuator and they derive asymptotic stability conditions subject to actuator saturation. Other PID controller design problems are considered in [S58], [S59]. In [S58], the authors introduce an LQ control design problem with event-based sampling. PI control synthesis with a relative threshold strategy is

proposed in [S59].

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4 Biography

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